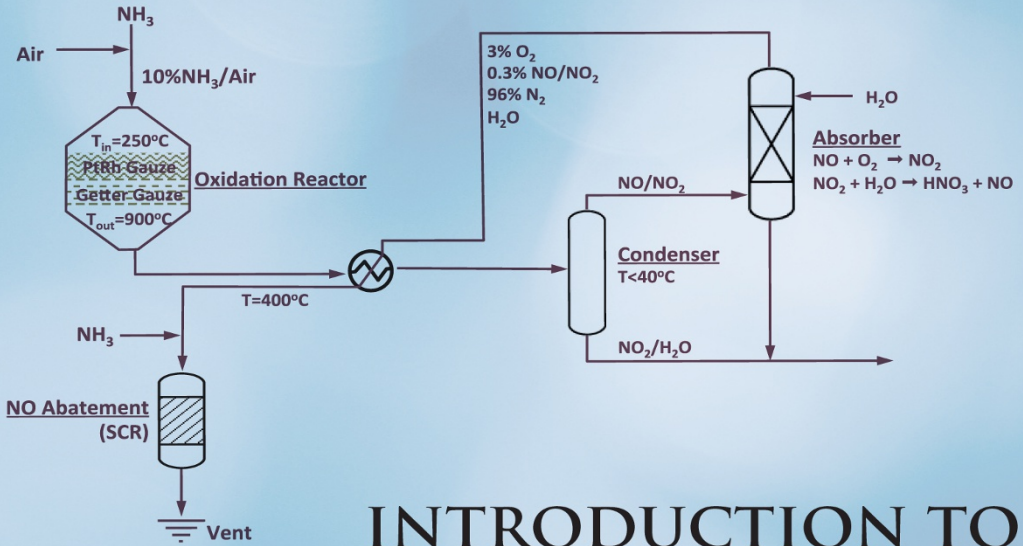




ROBERT J. FARRAUTO
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INTRODUCTION TO CATALYSIS AND INDUSTRIAL CATALYTIC PROCESSES

*INTRODUCTION
TO CATALYSIS
AND INDUSTRIAL
CATALYTIC PROCESSES*

INTRODUCTION TO CATALYSIS AND INDUSTRIAL CATALYTIC PROCESSES

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To my loving wife, friend, and critic, Karen, of over 49 years, who has supported me in all good things and forgiven my faults and mistakes; my 5 children and 10 grandchildren who have brought me mostly joy, been a constant source of fun and entertainment, and have given me understanding, support, love, excitement, inspiration, and challenges that have led to my growth; my loving, supportive brothers and sisters (all 7); and my dad and mom who taught me to love learning, life, and the Christian way. I especially dedicate this work (an offspring of our earlier book) to my son Charles who died unexpectedly on September 25, 2014 and who greatly touched and brightened the lives of his family, friends, and coworkers.

Calvin H. Bartholomew

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PREFACE

“Simplicity is the ultimate sophistication.”

THese words of Leonardo da Vinci were recently quoted by Steve Jobs of Apple in the book by Walter Isaacson. *Simplicity* was the first guiding principle in the preparation of this introductory book. The second guiding principle was to *share our considerable industrial and academic experience* in working with and teaching about catalysis fundamentals and industrial catalytic processes.

All of us authors have worked in industry and academia, two of us as technical consultants. Dr. Farrauto was affiliated with BASF (formerly Engelhard), Iselin, New Jersey for 37 years having worked in environmental, chemical, petroleum, and alternative energy fields and is now Professor of Practice in the Earth and Environmental Engineering Department at Columbia University in the City of New York. Dr. Dorazio, a research engineer at BASF (New Jersey), has worked in catalysis research and in scale-up of catalysts for the chemical, petroleum, and environmental fields. He is also Adjunct Professor in the Chemical Engineering Department at New Jersey Institute of Technology (NJIT). Dr. Bartholomew, Professor Emeritus in the Chemical Engineering Department at Brigham Young University, Provo, Utah, worked for a year at Corning Glass (with Dr. Farrauto) in auto emissions control after which he taught and conducted research and consulting for 41 years in catalyst design/deactivation and reactor/process design for environmental cleanup and synthetic fuel production. He continues to be active in writing, teaching short courses, and consulting. All of us have been widely engaged in various degrees of teaching industrial catalysis at the undergraduate and graduate levels. Bartholomew and Farrauto have coauthored the widely used text and reference book entitled “Fundamentals of Industrial Catalytic Processes,” a more advanced, in-depth version of the topics in the current book and a likely sequel to this book.

Industrial catalytic applications are seldom taught in undergraduate chemistry and chemical engineering programs, a surprising fact, given the large number of commercial processes that utilize catalysis. Thus, we accepted the challenge of writing a book that would introduce senior level undergraduates and new graduate students to this exciting field of catalytic processes, which is fundamental to chemical engineering and chemistry as practiced in industry. The need for a thorough understanding of fundamental principles of chemistry and catalysis is given. The transition of this knowledge to their commercial applications is our objective, especially for the many chemistry and chemical engineering students who spend much of their careers working in industry with catalytic processes. We also include the many professionals of varying disciplines

who suddenly find themselves with a new assignment of working on a catalytic process without previous training in the basics of catalysis and catalytic processes.

Our goal is to explain the fundamental principles of catalysis and their applications of catalysis in a simple, introductory textbook that excites those contemplating an industrial career in chemical, petroleum, alternative energy, and environmental fields in which catalytic processes play a dominant role. The book focuses on non-proprietary, basic chemistries and descriptions of important, currently used catalysts and catalytic processes. Considerable practical examples, recommendations, and cautions located throughout the book are based on authors' experience gleaned from teaching, research, commercial development, and consulting, including feedback from many students and associates. Suggested readings (reviews, books, and journal articles) are included at the end of each chapter to encourage interested readers to deepen their knowledge of these topics. Process diagrams have been simplified to provide an overview of principal process units (e.g., reactors and separation units) and important process steps, including reactant and product streams. Nevertheless, it should be recognized that commercial engineering process flow sheets include many other details and specifications, for example, piping, pumps, valves, heat exchangers, and other process equipment needed to operate and control the plant, including special equipment for plant start-up, catalyst pretreatment, purges, safety, regeneration, and so on.

Chapters 1–5 introduce the reader to basic principles of catalysis, including reaction kinetics, simple reactor design concepts, and catalyst preparation, characterization, and deactivation. Accompanying each chapter are questions and suggested readings. Chapters 6–15 describe by category applications and practice in the industry, including process chemistry, conditions, catalyst design, process design, and catalyst deactivation problems for each catalytic process. Chapter 6 describes hydrogen and syngas generation processes for different end applications. Processes for the synthesis of ammonia, methanol, and hydrocarbon liquids (Fischer–Tropsch process) are presented in Chapter 7. Processes for selective catalytic oxidation to (a) commodity chemicals, including nitric, cyanic, and sulfuric acids, formaldehyde, and ethylene oxide, and (b) specialized products such as acrylic acid, maleic anhydride, and acrylonitrile are presented in Chapter 8. Catalytic processes for hydrogenation of vegetable oils, olefins, and functional groups for highly specialized products are presented in Chapter 9. Catalytic processes in refining of petroleum to fuels are presented in Chapter 10. Selected commercial processes utilizing (a) homogeneous catalysts, (b) commercial enzymes, and (c) polymerization catalysts are described in Chapter 11. Chapters 12, 13, and 14 summarize features of important processes for catalysts used in environmental control of gaseous emissions from (a) stationary sources (e.g., power plants) and mobile sources, including (b) gasoline- and (c) diesel-fired vehicles. The final chapter 15 gives a brief summary of (1) catalytic processes for production of bio diesel and ethanol fuels from edible biomass which will ultimately find application to production of similar fuels from non-edible cellulosic biomass and (2) catalyst technology for the emerging hydrogen economy with emphasis on fuel cell technology.

New York, New York
Iselin, New Jersey
Provo, Utah
22 November 2015

Robert J. Farrauto
Lucas Dorazio
Calvin H. Bartholomew

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NOMENCLATURE

SYMBOLS

| | |
|-------------------------|--|
| A | Frontal area (m^2) |
| a_s | Geometric surface area = ratio of surface area to volume (m^{-1}) |
| a_{Sh} | Fitted parameter used for mass transfer coefficient |
| B | Integral breadth (Scherrer's formula) ($^\circ$) |
| C | Concentration (mol/m^3) |
| C_{BET} | BET constant |
| C_{WP} | Weisz–Prater criterion |
| D | Diffusivity (m^2/s) |
| D_e | Effective diffusivity (m^2/s) |
| D_k | Knudsen diffusivity (m^2/s) |
| d_p | Particle diameter (d_h) = monolith channel diameter (m) |
| d_{pore} | Pore diameter (m) |
| E_A | Activation energy (J/mol) |
| E_{cell} | Net voltage of fuel cell (V) |
| E_{cell}° | Standard state cell voltage (V) |
| E_o | Standard state voltage in the Nernst equation (V) |
| f | Friction factor |
| F | Molar flow (mol/s) |
| F_c | Faraday constant (C/V) |
| g_c | Gravitational constant (m/s^2) |
| GHSV | Gas hourly space velocity (h^{-1}) |
| ΔG_{rxn} | Free energy change during reaction (J/mol) |
| H | Henry's law constant |
| ΔH_{rxn} | Enthalpy change during reaction (J/mol) |
| J | Molar flux ($\text{mol}/(\text{m}^2 \text{ s})$) |
| k | Reaction rate constant ($\text{mol}/(\text{s l})$) |
| K_{eq} | Equilibrium constant |
| k_f, k_d | Rate constants for absorption and desorption ($\text{mol}/(\text{s l})$) |
| k_{MT} | Mass transfer coefficient (m/s) |
| k_o | Pre-exponential factor (g) |
| M_{flow} | Mass flow rate (kg/h) |
| MW | Molecular weight (mol/g) |
| n | Number of electrons transferred |
| N_A | Avogadro's number (mol^{-1}) |
| P | Pressure (atm) |
| P_i | Partial pressure of species i (atm) |

xxviii NOMENCLATURE

| | |
|-------------------------|--|
| P_o | Saturation pressure (atm) |
| r | Reaction rate per unit volume (mol/(s l)) |
| r' | Reaction rate per unit mass (mol/(s g)) |
| R | Ideal gas constant (J/(mol K)) |
| Re | Reynolds number |
| r_k | Rate of reaction on catalyst surface (mol/(s l)) |
| r_{MT} | Rate of bulk diffusion (mol/(s l)) |
| $r_{MT,g}$ | Rate of bulk diffusion through gas phase (mol/(s l)) |
| $r_{MT,g-l}$ | Rate of diffusion through gas-liquid interface (mol/(s l)) |
| $r_{MT,l-s}$ | Rate of diffusion through liquid-solid interface (mol/(s l)) |
| r_p | Pore radius (m) |
| R_{pellet} | Radius of catalyst pellet (m) |
| r_{pore} | Rate of pore diffusion (mol/(s g)) |
| Sc | Schmidt number |
| Sh | Sherwood number |
| ΔS_{rxn} | Entropy change during reaction (J/K) |
| SV | Space velocity (h^{-1}) |
| t | Residence time (min or h) |
| T | Temperature ($^{\circ}\text{C}$ or K) |
| t_{crys} | Thickness of crystallite (Scherrer's formula) (nm) |
| u | Bulk stream velocity (m/s) |
| V | Reactor volume (m^3) |
| V_{ad} | Volume adsorbed at P (m^3) |
| V_{flow} | Volumetric flow (m^3/s) |
| V_m | Molar volume (mol/m^3) |
| V_{mono} | Adsorbed volume at monolayer coverage (m^3) |
| v_o | Volumetric flow rate (m^3/h) |
| V_{rxtr} | Reactor volume (m^3) |
| W_{cat} | Catalyst mass (g) |
| $WHSV$ | Weight hourly space velocity (h^{-1}) |
| X | Fractional conversion |
| x_{Sh} | Fitted parameter used for mass transfer coefficient |
| Z | Reactor length (m) |

GREEK SYMBOLS

| | |
|-----------------|---|
| β | Approach to equilibrium |
| γ | Surface tension (N/m) |
| δ_M | Thickness of mass transfer boundary layer (m) |
| ε | Binary interaction energy (K) |
| ε | Void fraction in the bed |
| ε_p | Particle porosity |
| θ | Contact angle ($^{\circ}$) |
| θ_d | Bragg angle ($^{\circ}$) |